22.033 Core Group- Reactor Core and Secondary Design

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Overview

Proposed Design & Specs

• Core

Secondary

Next Steps
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Preliminary Design

 Lead Cooled Fast Reactor with Supercritical CO₂ Secondary Loop

- 1000 MWt (~450 MWe)
 - Limited by velocity of LBE (2.5-3 m/s) currently we are using 2.5 m/s
 - Subject to changes as ΔT and flow area changes (working on upping it to ~1200 MWt)

Preliminary Design



- Black- Fuel Regions (UO₂)
- Purple- Control Rods (B₄C)
- Beige-Reflector (MgO)
- Red- Shield (B₄C)
- Orange- Coolant (LBE)
- Note the Blue containment is not the actual containment (in reality it is larger)

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Core Design Process

- Used MCNP (Monte Carlo N-Particle) code to design reactor
- Based off of other similar hexagon core shaped liquid metal cooled reactors (STAR-LM, ELSY)
- Design Iterations

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- Version 1.0, looked at a lot of reference designs and created something similar
- See if it were critical
- Fuel Pin design: fuel → LBE gap → protective clad → T91
 → protective clad → coolant
- It had the whole range of S/D with rods in and supercritical with rods out
 - Needed less reactivity at top of core (helps with S/D margin)
 - Needed less power peaking in the middle

Control Rods	Keff (+- 0.0005)	
In	0.96822	
25% out	1 01184	
50% aut	1.01104	
50% Out	1.08764	
75% out	1.11812	
Full Out	1.3265	



- Added Axial Zoning to fix the large excess reactivity (20% enriched Lower, 15% enriched Middle, 10% enriched bottom)
- Added Radial Zoning to get a flatter flux profile (Added 5% to the outer rings)

Control Rods	In	0.25	0.5	0.75	Out
Keff	0.95387	1.08059	1.15039	1.16142	1.16144



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- Purple- Control Rods (B₄C)
- Beige-Reflector (MgO)
- Red- Shield (B₄C)
- Orange- Coolant (LBE)
- Blue- Cladding (T91 stainless steel, protective outer layer)
- Note the Blue containment is not the actual containment (in reality it is larger)





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Iteration 2

Power Calculation

• Used Power= $\dot{m} c_p \Delta T$

• Where $\dot{m} = \rho v A$

Where v is limited at 2.5 m/s, rho is 10500 kg/m³, A is the cross sectional coolant flow area, c_p is 150 J/kg·K and ΔT is the temperature change across the core

Directly proportional to A and ΔT

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Decay Heat Removal

- After a month of shutdown from long operation still producing about 3 MWt of energy
- After a month of shutdown from 1 month of operation still producing 400 kWt of energy
- Need to see how much power produced is sufficient to keep LBE liquid and then work with process heat

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Secondary System

Modeled in EES

Temperature and mass flow calculations

- Initial Assumptions Made
 - Heat exchanger input and output for S-CO₂
 - Low end temperature after condenser

Allows for faster optimization in the future

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Secondary System



Secondary System

- More S-CO₂ data required to perform analysis of pressure changes.
 - Enthalpy Tables
- Possible second loop with an added re-heater and compressor to account for changes in specific heat
- Energy diverted to Process-Heat needs to be accounted for

Only majorly effects electricity generated

Brayton Cycle: Quick Overview



http://chemwiki.ucdavis.edu/@api/deki/files/13235/=TS_Curve.jpg

LBE & S-CO₂ Heat Exchanger





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 Printed Circuit Heat Exchanger (PCHE) vs. Shelland-Tube Heat Exchanger



- Compact design
- Competitive Efficiency
- Friction Factor for LBE becomes obstacle

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Shell-and-Tube Heat Exchanger



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- Simple design (easy to make, low cost, etc.)
- Larger than PCHE
- Competitive efficiency

http://www.thermopedia.com/content/1211/?tid=104&sn=1410

Next Step

 Secondary: Better data, more accurate values, possible second re-heater/compressor loop, and process heat removal

 Core: Natural Circulation, Decay heat work, continue optimizing core zoning, thermal analysis of fuel

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QUESTIONS?

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